

Second order system

Sources of second order dynamics in the chemical industries come from a series of first-order systems, or a processing system with a controller.

For input step change of magnitude of a , $u(s) = a/s$ we have:

$$y(s) = \frac{k_p a}{s(\tau^2 s^2 + 2\tau\zeta s + 1)} \equiv \frac{k_p a / \tau^2}{s(s - p_1)(s - p_2)}$$

where

$$p_1 = -\frac{\zeta}{\tau} + \frac{\sqrt{\zeta^2 - 1}}{\tau} \quad p_2 = -\frac{\zeta}{\tau} - \frac{\sqrt{\zeta^2 - 1}}{\tau}$$

Case

A: (over-damped) when $\zeta > 1$, we have two distinct and real poles

$$y(t) = k_p a \left[1 - e^{-\zeta t / \tau} \left(\cosh(\sqrt{\zeta^2 - 1} \frac{t}{\tau}) + \frac{\zeta}{\sqrt{\zeta^2 - 1}} \sinh(\sqrt{\zeta^2 - 1} \frac{t}{\tau}) \right) \right]$$

Case B: (critically-damped) when $\zeta = 1$, we have two equal poles

$$y(t) = k_p a \left[1 - \left(1 + \frac{t}{\tau} \right) e^{-t / \tau} \right]$$

Case C: (under-damped) when $\zeta < 1$, we have two complex conjugate poles

$$y(t) = k_p a \left[1 - \frac{1}{\sqrt{\zeta^2 - 1}} e^{-t\zeta / \tau} \sin(\omega t + \phi) \right]$$

2nd order system is oscillate depending on value of damping factor ζ :

If $\zeta > 1$ then the system is not oscillation

If $\zeta = 1$ then the system is critical damped

If $\zeta < 1$ then the system is oscillation with damping

If $\zeta = 0$ then the system is continuous oscillation

And if ζ is -ve then the system is diverged oscillation

If ζ is +ve then the system is stable

The dynamic response for all cases is shown in Figure below

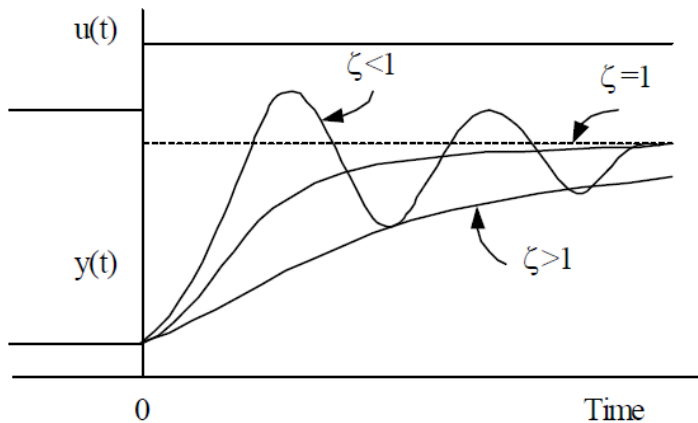


Fig.24 The response of second order system to step change

- The over-damped response is sluggish and resembles a little the response of a first-order system and becomes more sluggish with larger values of ζ .
- The critically damped response is faster than the over-damped one.
- The under-damped response is faster than the others, but oscillates. The oscillatory behavior becomes pronounced with smaller values ζ .

Typical 2nd order oscillatory system, simple manometer

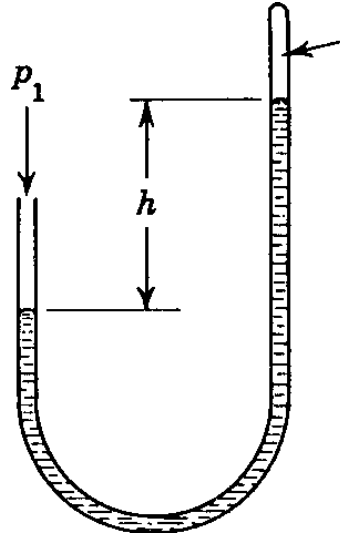


Fig.25 Manometer system

Manometer (momentum balance)

Balance of forces on the system=mass of system \times acceleration

Since acceleration = $\frac{d(\text{velocity})}{dt}$

(Force due to pressure p_1 on lag₁) – (force due to pressure p_2 on lag₂) – (force due to liquid level difference in the two lags) – (force due to fluid friction) =(mass of liquid in the tube) \times (acceleration)

$$p_1 A_1 - p_2 A_2 - (h) A_2 \rho g - (\text{force due to fluid friction}) = m \frac{dv}{dt} \quad (1)$$

$$(\text{force due to fluid friction}) = \Delta p \pi R^2 = A \frac{8\mu L}{R^2} \frac{dh}{dt} \quad (2)$$

$$v = \frac{dh}{dt} \text{ and } \frac{dv}{dt} = \frac{d^2 h}{dt^2} \quad (3)$$

Put eq.(2) and (3) in eq.(1)

$$\Delta p A - \rho g A h - \frac{8\mu L A}{R^2} \frac{dh}{dt} = \rho A L \frac{d^2 h}{dt^2}$$

$$\left(\frac{L}{g}\right) \frac{d^2 h}{dt^2} + \frac{8\mu L}{\rho g R^2} \frac{dh}{dt} + h = \frac{1}{\rho g} \Delta p$$

$$\tau^2 \frac{d^2 h}{dt^2} + 2\zeta\tau \frac{dh}{dt} + h = k\rho$$

$$\frac{h(s)}{p(s)} = \frac{k}{\tau^2 s^2 + 2\zeta\tau s + 1}$$

$$\tau^2 = \frac{L}{g} \quad , \tau = \sqrt{\frac{L}{g}} \quad , 2\zeta\tau = \frac{8\mu L}{\rho g R^2} \quad , k = \frac{1}{\rho g}$$

$$\zeta = \frac{4\mu}{\rho R^2} \sqrt{\frac{L}{g}}$$

$$\text{If } \zeta \geq 1$$

$$\frac{4\mu}{\rho R^2} \sqrt{\frac{L}{g}} \geq 1$$